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**IN THE CLAIMS:**

Claims 1-36 (Cancelled)

- 1 37. (Previously presented) A direct oxidation fuel cell, comprising
- 2 (A) a catalyzed membrane electrolyte, having an anode aspect and a cathode
- 3 aspect;
- 4 (B) a fuel cell housing enclosing said fuel cell with an anode chamber being
- 5 defined between said anode aspect of the catalyzed membrane electrolyte and an exterior
- 6 portion of said cell housing;
- 7 (C) a direct fuel feed into an anode chamber that has no liquid exit port such
- 8 that liquid that is present in said anode chamber cannot exit said anode chamber except
- 9 across said catalyzed membrane electrolyte;
- 10 (D) at least one gaseous effluent release port located in said anode chamber in
- 11 close proximity to said anode aspect of the catalyzed membrane electrolyte; and
- 12 (E) a load coupled across said fuel cell, providing a path for electrons pro-
- 13 duced in electricity generating reactions of said fuel cell.
- 1 38. (Previously presented) The direct oxidation fuel cell as defined in claim 37
- 2 wherein a substance delivered by said direct fuel feed into said liquid-closed volume in
- 3 the anode chamber is up to 100% fuel.
- 1 39. (Previously presented) The direct oxidation fuel cell as defined in claim 38
- 2 wherein said fuel is methanol.
- 1 40. (Previously presented) The direct oxidation fuel cell as defined in claim 37
- 2 wherein fuel is delivered by said direct fuel feed into said anode chamber without anode
- 3 liquid recirculation.

1 41. (Previously presented) The direct oxidation fuel cell as defined in claim 37  
2 wherein water produced at said cathode is not actively collected or pumped to said anode  
3 chamber.

1 42. (Previously presented) The direct oxidation fuel cell wherein gaseous effluent  
2 traveling out of said fuel cell through said gaseous effluent release port is at least partially  
3 comprised of carbon dioxide.

1 43. (Previously presented) The direct oxidation fuel cell as defined in claim 37  
2 wherein at least a portion of one wall of said anode chamber is gas permeable and liquid  
3 impermeable.

1 44. (Previously presented) A direct oxidation fuel cell, comprising:  
2 (A) a catalyzed membrane electrolyte having an anode aspect and a cathode  
3 aspect;  
4 (B) a fuel cell housing with an anode chamber being defined between said an-  
5 ode aspect of said catalyzed membrane electrolyte and an exterior portion of said cell  
6 housing, and fuel being delivered to, but not actively recirculated from, said anode cham-  
7 ber; and  
8 (C) gaseous anodic product removal component disposed between said cata-  
9 lyzed membrane electrolyte and said housing.

1 45. (Previously presented) A direct oxidation fuel cell system, comprising:  
2 (A) a direct oxidation fuel cell having:  
3 (i) a catalyzed membrane electrolyte, having an anode aspect and a  
4 cathode aspect;  
5 (ii) a fuel cell housing enclosing said fuel cell with an anode chamber  
6 being defined between said anode aspect of the catalyzed membrane electrolyte and an  
7 exterior portion of said cell housing;

1 46. (Previously presented) A direct oxidation fuel cell, comprising:

2 (A) a catalyzed membrane electrolyte assembly having an anode aspect and a

3 cathode aspect and

4 (B) means for outporting gasses away from the anode aspect of the fuel cell

5 which means for outporting gasses is disposed in close proximity to said anode aspect of

6 the catalyzed membrane electrolyte assembly.

1 47. (Withdrawn) A gas management component for use in a direct oxidation fuel  
2 cell having a catalyzed membrane electrolyte with an anode aspect and a cathode aspect,  
3 comprising:  
4 an element substantially comprised of a gas-permeable, liquid-  
5 impermeable material, which element is disposed in close proximity to the anode aspect  
6 of the catalyzed membrane electrolyte assembly.

1 48. (Withdrawn) The gas management component as defined in claim 47 wherein  
2 said material is gas-selective in such a manner that it is permeable to anodic effluent gas,  
3 but is substantially less permeable to oxygen.

1 49. (Withdrawn) The gas management component as defined in claim 47 wherein  
2 said gas management component is made part of a flow field element, providing said  
3 flow field element with gas releasing properties while effectively delivering fuel to active  
4 area of the membrane electrolyte. .

1 50. (Withdrawn) The gas management component as defined in claim 49 wherein  
2 fuel is delivered to said active area of the membrane electrolyte through an associated  
3 anodic diffusion layer.

1 51. (Withdrawn) The gas management component as defined in claim 49 wherein  
2 said flow fields encourage removal of anodically-generated gasses such that they are re-  
3 leased from the direct oxidation fuel cell prior to excessive collection of gaseous anodic  
4 product within the said anode chamber in said fuel cell.

1 52. (Withdrawn) The gas management component as defined in claim 47 wherein  
2 said gas management component is disposed within said fuel cell in such a manner that  
3 anodically-generated gasses are released prior to coalescing and impeding the flow of  
4 fuel from an associated fuel source into said anode chamber.

1 53. (Withdrawn) A membrane electrode assembly of a direct oxidation fuel cell,  
2 comprising:  
3 (A) a protonically-conductive, electronically non-conductive catalyzed mem-  
4 brane electrolyte;

5 (B) a catalyst disposed on said membrane electrolyte;  
6 (C) an anode diffusion layer disposed contiguous to an anode aspect of the  
7 membrane electrolyte;  
8 (D) a cathode diffusion layer disposed contiguous to a cathode aspect of the  
9 membrane electrolyte; and  
10 (E) a gas-permeable, liquid-impermeable layer coupled to, or in close prox-  
11 imity with said anode diffusion layer.

1 54. (Withdrawn) The membrane electrode assembly as defined in claim 53 wherein  
2 said gas-permeable, liquid-impermeable layer is mechanically attached or bonded to said  
3 anode diffusion layer.

1 55. (Previously presented) A direct oxidation fuel cell comprising:  
2 (A) a membrane electrode assembly, including:  
3 (i) a protonically-conductive, electronically non-conductive catalyzed  
4 membrane electrolyte;  
5 (ii) a catalyst disposed on said membrane electrolyte;  
6 (iii) an anode diffusion layer disposed contiguous to an anode aspect of  
7 the membrane electrolyte;  
8 (iv) a cathode diffusion layer disposed contiguous to a cathode aspect  
9 of the membrane electrolyte; and  
10 (B) a gas-permeable, liquid-impermeable layer coupled to said anode diffusion  
11 layer; and  
12 (C) a coupling across said fuel cell to conduct electricity generated by said  
13 fuel cell to an associated load; and  
14 (D) a fuel cell housing substantially enclosing said fuel cell.

1 56. (Previously presented) A direct oxidation fuel cell system, comprising:  
2 (A) a fuel source;  
3 (B) a direct oxidation fuel cell including:

4

5 (i) a protonically-conductive, electronically non-conductive catalyzed  
6 membrane electrolyte;

7 (ii) a catalyst disposed on said membrane electrolyte;

(iii) an anode diffusion layer disposed contiguous to the anode aspect of the membrane electrolyte;

10 (iv) a cathode diffusion layer disposed contiguous to the cathode aspect  
11 of the membrane electrolyte; and

12 (v) a gas-permeable, liquid-impermeable layer coupled to said anode  
13 diffusion layer; and

14 (vi) a coupling across said fuel cell to conduct electricity generated by  
15 said fuel cell to an associated load.

1 57. (Currently Amended) The direct oxidation fuel cell system as defined in claim 56  
2 wherein the fuel is up to 100% fuel.

1 58. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 57 wherein said fuel is methanol.

1 59. (Withdrawn) A method of managing anodic effluent in a direct oxidation fuel  
2 cell, said fuel cell having a catalyzed membrane electrolyte with an anode aspect and a  
3 cathode aspect, the method including the step of:

removing gaseous anodic effluent from a liquid by providing a gas management component comprised substantially of a gas-permeable, liquid-impermeable layer disposed in close proximity to the anode aspect of the direct oxidation fuel cell.

1 60. (Withdrawn) The method, as defined in claim 59, including providing said gas-  
2 permeable, liquid-impermeable layer in contact with the anode aspect of the membrane  
3 electrolyte assembly.

1 61. (Withdrawn) A method of separating anodically-generated gasses in a direct  
2 oxidation fuel cell, said fuel cell having a catalyzed membrane electrolyte with an anode  
3 aspect and a cathode aspect, and an anode chamber being defined between said anode  
4 aspect and an exterior of said fuel cell, the method including the steps of:

5 separating said anodically-generated gasses from a fluid volume of fuel contained  
6 within said anode chamber of said fuel cell, without recirculating said volume of fuel.

1 62. (Previously presented) A direct oxidation fuel cell system, comprising:

2 (A) a fuel source;

3 (B) a direct oxidation fuel cell having a catalyzed membrane electrolyte with  
4 an anode aspect and a cathode aspect;

5 (C) a cell housing with an anode chamber defined between the anode aspect of  
6 the catalyzed membrane and one exterior portion of said cell housing, with said chamber  
7 having no exit port for liquid;

8 (D) an element disposed between said fuel source and said anode aspect of the  
9 direct oxidation fuel cell for controlling the delivery of fuel to the direct oxidation fuel  
10 cell system.

1 63. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 62, wherein said element controls the delivery of fuel without pumps or active recircula-  
3 tion mechanisms.

1 64. (Withdrawn) The direct oxidation fuel cell system as defined in claim 62 wherein  
2 said fuel source is substantially entirely disposed within said fuel cell.

1 65. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 62 wherein  
3 said fuel source is disposed external to the fuel cell.

1 66. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 62 wherein

3 a pressure differential exists between the fuel in the fuel source and the anode  
4 chamber of the fuel cell.

1 67. (Withdrawn) The direct oxidation fuel cell system as defined in claim 62 wherein  
2 said element for controlling fuel delivery includes a pump.

1 68. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 62 wherein

3 said fuel source contains more than one liquid that may be mixed between the fuel  
4 source and the anode of the fuel cell.

1 69. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 68 wherein

3 said fuel source contains methanol and water.

1 70. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 62 wherein

3 said fuel source is capable of delivering up to 100% fuel to said fuel cell.

1 71. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 70 wherein said fuel is methanol.

1 72. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 62 wherein

3 delivery of said fuel is performed by suction.

1 73. (Previously presented) The direct oxidation fuel cell system as defined in claim  
2 62 wherein

3           said delivery by suction is performed by the action of a capillary network in a po-  
4    rous component, which is disposed between said fuel source and said anode of said direct  
5    oxidation fuel cell.

1   74.   (Withdrawn) A method of delivering fuel to a direct oxidation fuel cell compris-  
2    ing the steps of delivering fuel to the anode of the fuel cell in such a manner that the vol-  
3    ume of fuel that has been consumed at the anode of the fuel cell is replaced by the same  
4    volume of fresh fuel or a fuel and water mixture delivered from a fuel source.

1   75.   (Withdrawn) A method of controlling delivery of fuel to a direct oxidation fuel  
2    cell system wherein said fuel cell system includes a fuel source, a direct oxidation fuel  
3    cell having a catalyzed membrane electrolyte with an anode aspect and a cathode aspect  
4    and an anode chamber being defined between said anode aspect and an exterior portion of  
5    said direct oxidation fuel cell, said anode chamber not having a port by which liquid can  
6    exit the anode chamber, the method including the steps of:

7           providing a mass transport controlling element disposed between the anode aspect  
8    of the catalyzed membrane and said fuel source whereby fuel delivery to the fuel cell  
9    system is controlled without pumps or recirculation components.

1   76.   (Withdrawn) The method as defined in claim 75 including the further step of  
2       disposing said fuel source entirely within said fuel cell.

1   77.   (Withdrawn) The method as defined in claim 75 including the further step of  
2       disposing said fuel source external to the fuel cell.

1   78.   (Withdrawn) The method as defined in claim 75 including the further step of  
2       placing fuel in said fuel source under a slight pressure to induce a pressure differ-  
3       ential between the fuel in said fuel source and the fuel in the anode chamber of the fuel  
4       cell.

1 79. (Withdrawn) The method as defined in claim 75 including the further step of  
2 providing in said fuel source more than one liquid; and  
3 mixing said liquids between the fuel source and the anode chamber of the fuel  
4 cell.

1 80. (Withdrawn) The method as defined in claim 79 wherein said liquids provided to  
2 said fuel source include methanol and water.

1 81. (Withdrawn) The method as defined in claim 75 including providing as said fuel,  
2 a substance of up to 100% methanol.

1 82. (Withdrawn) The method as defined in claim 81 wherein said fuel substance is  
2 methanol.

1 83. (Withdrawn) The method as defined in claim 75 including the further step of de-  
2 livering said fuel to said anode chamber by suction.

1 84. (Withdrawn) The method as defined in claim 75 including the further step of de-  
2 livering fuel from said fuel source to said anode by the suction action of a capillary net-  
3 work in a porous component that is disposed between said fuel source and said anode  
4 chamber of said direct oxidation fuel cell.